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Chapter 1

1.1 Process classification

Classify the following processes as batch, continuous, or Semibatch, and transient or steady-state.

- A balloon is being filled with air at a steady rate of 2 g/min. (Answer: Semibatch)
- A bottle of milk is taken from the refrigerator and left on the kitchen table. (Answer: Batch, transient in heat).
- Carbon monoxide and steam are fed into a tubular reactor at a steady-rate and react to form carbon dioxide and hydrogen. Products and unused reactants are withdrawn at the other end. The reactor contains air when the process is started up. The temperature of the reactor is also constant, and the composition and flow rate of the entering reactant stream are independent of time. Classify the process initially (Answer: Continuous, transient) and after a long period has elapsed (Answer: Continuous, steady state).

1.2 Types of processes

Water ($\rho = 1000 \text{ kg/m}^3$) enters a 2.00 m^3 tank at a rate of 6.00 kg/s and is withdrawn at a rate of 3.00 kg/s . The tank is initially half-full.

- Is the process continuous, batch or semi-batch? (Answer: Continuous)
- Is it transient or steady-state? (Answer: Transient)
- Use the general material balance equation to determine how long it will take the tank to overflow. (Answer: $1000 \text{ kg}/(3 \text{ kg/s})$)

Solution:

Mass of water in the tank = $2.0 \text{ m}^3 (1000 \text{ kg/m}^3) = 2000 \text{ kg}$

The tank is half full $2000 \text{ kg}/2 = 1000 \text{ kg}$

The time necessary to fill the tank = $1000 \text{ kg} / (3 \text{ kg/s}) = 333.3 \text{ sec}$

1.3 Unit conversion

How many seconds are in a year? (3600 s/h, 24 hours/day, 365 days/year).

Solution:

$$\cancel{\text{year}} \left| \frac{365 \cancel{\text{days}}}{\cancel{\text{year}}} \right| \left| \frac{24 \cancel{\text{h}}}{\cancel{\text{day}}} \right| \left| \frac{3600 \text{s}}{\cancel{\text{h}}} \right|$$

There is 3.1536E7 seconds/year

1.4 Flowrate through horizontal pipe

Natural gas is flowing through a horizontal pipe at a flowrate of $50 \text{ ft}^3/\text{s}$. What is this flowrate in m^3/s , gal/hr? (Use conversion table)

Solution:

$$\text{Flow rate in } \text{m}^3 = (50 \text{ ft}^3/\text{s})(1 \text{ m}^3/35.3145 \text{ ft}^3) = 1.41585 \text{ m}^3/\text{s}$$

$$\text{Flow rate in gal/hr} = (50 \text{ ft}^3/\text{s})(264.17 \text{ gal}/35.3145 \text{ ft}^3)(3600 \text{ s/h}) = 1.34649\text{E}6 \text{ gal/h}$$

1.5 Molar flow rate

Propane gas (C_3H_8) flows to a furnace at a rate of $1450 \text{ m}^3/\text{h}$ at 15°C and 150 kPa (gauge), where it is burned with 8% excess air. Calculate the molar flow rate (moles/s) of propane gas entering the furnace. (Hint: assume ideal gas and use $P\dot{V} = \dot{n}RT$)

Solution:

Using ideal gas law $P\dot{V} = \dot{n}RT$

$$\dot{n} = \frac{P\dot{V}}{RT}$$

$$P_{abs} = P_{gage} + P_{atm}$$

$$P_{abs} = 150 \text{ kPa} + 101.32 \text{ kPa}$$

$$P_{abs} = 251.32 \text{ kPa}$$

$$\dot{n} = \frac{(251.32 \text{ kPa}) \left| \frac{1000 \text{ Pa}}{\text{kPa}} \right| (1450 \text{ m}^3/\text{h}) \left| \frac{\text{h}}{3600 \text{ s}} \right|}{8.314 \frac{\text{m}^3 \cdot \text{Pa}}{\text{mol} \cdot \text{K}} (15 + 273 \text{ K})}$$

$$n: \text{ number of moles} = 42.2218 \text{ mol/s}$$

1.6 Dimensional homogeneity

A quantity k depends on the temperature T in the following manner:

$$k \left(\frac{\text{mol}}{\text{cm}^3 \cdot \text{s}} \right) = A \exp \left(- \frac{E_a}{R T} \right)$$

The units of the quantity E_a are cal/mol, and T is in K (Kelvin). What are the units of A and

R . (hint: note that the exponent is of unitless values; $E_a / RT = []$).

Solution:

The units of A [=] mol/cm³s

R [=] cal/mol.K

1.7 Calculation of mass for specific gravity and volume

The specific gravity of gasoline is approximately 0.7. What is the mass (kg) of 10 liters of gasoline? (Answer: 7 kg)

Solution:

Mass = density * volume

$$\text{Mass} = (0.7 \text{ kg/L}) * 10 \text{ L} = 7 \text{ kg}$$

1.8 Convert of equation to other units

The heat capacity of ammonia, $C_p = 2.5 \text{ J/g} \cdot ^\circ\text{C}$. Convert the expression for C_p to $\text{Btu}/(\text{lb}_m \cdot ^\circ\text{F})$. (Hint: note that the $^\circ\text{C}$ and $^\circ\text{F}$ here is the difference in temperature;

$$\left. \frac{1 \text{ } ^\circ\text{C}}{1.8 \text{ } ^\circ\text{F}}; \frac{1 \text{ K}}{1.8 \text{ } ^\circ\text{R}}; \frac{1 \text{ } ^\circ\text{C}}{1 \text{ K}}; \frac{1 \text{ } ^\circ\text{C}}{1 \text{ K}} \right).$$

Answer:

$$C_p = 2.5 \frac{\text{J}}{\text{g} \cdot ^\circ\text{C}} \left| \frac{453.593 \text{ g}}{1 \text{ lbm}} \right| \left| \frac{9.486 \times 10^{-4} \text{ Btu/s}}{1 \text{ J/s}} \right| \left| \frac{1 \text{ } ^\circ\text{C}}{1.8 \text{ } ^\circ\text{F}} \right|$$

$$C_p = 0.597609 \frac{\text{Btu}}{\text{lbm} \cdot ^\circ\text{F}}$$